ASX ANNOUNCEMENT
7 August 2025
ASX | GT1

*Building the pre-eminent vertically integrated **Lithium** business in Ontario, Canada*

PILOTING OF SEYMOUR CONCENTRATE SUCCESSFULLY PRODUCES BATTERY GRADE LITHIUM HYDROXIDE

HIGHLIGHTS

- **GT1 with its Partner, Korean battery materials producer, EcoPro Innovation, have successfully produced battery grade Lithium Hydroxide, meeting benchmarked end user specifications from GT1's Seymour spodumene bulk sample**
- **600kg of Seymour concentrate processed through pilot scale facility confirming EcoPro Innovation process flowsheet, producing exceptional overall recoveries averaging >94%**
- **Battery grade 56.5% $LiOH.H_2O$ product achieved with low impurities readily acceptable under EcoPro Innovation's product specifications utilising conventional sulfation route flowsheet and EcoPro in-house process knowledge and IP**
- **Concentrated spodumene from Seymour highly amenable to various process steps indicating lower end of operational costs to remove required impurities**
- **Successful piloting program will be used in Pre-Feasibility Study (PFS) development and marketing samples for additional future offtake agreements**

Green Technology Metals Limited (**ASX: GT1**)(**GT1** or the **Company**), a Canadian-focused multi-asset lithium business, is pleased to provide an update on lithium hydroxide conversion piloting testwork completed for its 100%-owned Seymour lithium project, located in Ontario, Canada in conjunction with its partner EcoPro Innovation (**EcoPro**).

Element	LiOH		Li_2CO_3	Na	Ca	Mg	Fe	Zn	Cu	Cr	Si	S
Result	56.5%	mg/kg	4,889	14	0.1	0	0	0	0	0	0.1	9

Table 1: Results of Lithium Hydroxide Monohydrate Purity Analysis

"We are extremely pleased to receive the final report from our downstream development partner, EcoPro Innovation, on the successful production of battery grade Lithium Hydroxide Monohydrate using spodumene concentrate produced from our Seymour project.

This outcome is the result of over the past 12 months hard work from our team, beginning with the bulk sample extraction from Seymour, concentrated replicating our proposed concentrator flowsheet in a different province and then co-ordinating with EcoPro on their testwork program and piloting facility based in Pohang, South Korea. The concentrate was then tested, analysed and processed through the pilot facility to produce the final product. The results confirm the high quality of our ore and concentrate product and will be utilised in the development of the final design criteria for our PFS on the proposed lithium hydroxide conversion facility.

The advantage that GT1 has with such a proven partner in the conversion of raw materials into battery grade lithium chemicals is a partnership that is heavily underrated and undervalued. Together with GT1's mine and concentrator development expertise and EcoPro's knowledge in their area of conversion creates and extremely valuable and derisked development opportunity for Ontario and the North American EV market. "

- GT1 Managing Director, Cameron Henry

Summary

The company's partnering 'framework' agreement and strategic objectives entered into in October 2024 with partner EcoPro Innovation was to establish a combined supply chain from mine to chemical production. In accordance with the framework, 1 tonne of concentrate produced from the Seymour mine bulk sample was shipped to Pohang, South Korea for further testing and processing through EcoPro's pilot facility to produce battery grade chemicals. 600kg of this concentrate was then ran through the pilot plant to demonstrate the proposed process conditions that a scaled up processing facility would similarly replicate. From the 600kg processed approximately 1 tonne of Lithium Sulphate (Li_2SO_4) was produced that was then taken through the EcoPro Innovation process to produce battery grade Lithium Hydroxide LiOH at lab scale – replicating the same process at currently used in EcoPro's 2 x operating trains of 11kt & 13kt in Pohang.

The opportunity to complete testwork and piloting of the company's ore and concentrates with a downstream, partner again demonstrates the strategic nature of the partnership and the advantage GT1 has over competitors that don't have the ability, knowledge or capability. The company strongly believes having an integrated solution requires this ability to ensure that the downstream component is designed to ensure that the mine concentrates can be processed efficiently and cost effectively to end user requirements. This has now been completed at a pilot scale acceptable to finalise designs and confirm suitability of the product produced from Seymour to be converted into battery grade material.

Tailings and by-products have been analysed as part of the testwork process to confirm the suitability of waste streams for potential by-products. Samples have now been returned to Thunder Bay for further engagement and discussions with offtake partners for those products to determine suitability with further testwork to be completed for acceptance.

GT1 plans to undertake the next phase of piloting testwork using ore from its 100% owned Root Lithium project, once market conditions improve. A bulk sample of ore from Root Bay Pegmatite #1 was collected from surface by controlled blasting and bagging, late in 2024. The bulk sample material was transported to Thunder Bay, Ontario where it is readily available for future concentrate and hydroxide testwork.

Testwork

Benefits identified during the EcoPro Testwork:

1. Seymour concentrates have been proven to produce battery grade lithium hydroxide utilizing conventional processing techniques with low impurities ensuring strong conversion characteristics.
2. The concentrate product has a higher than normal calcium oxide (CaO) content which may provide for lower calcination temperatures to facilitate α-spodumene to β spodumene conversion which may result in lower energy input
3. Overall process recoveries are high and are expected to remain at or above industry standard recovery rates >90% at plant scale up – dependent on successful plant design characteristics
4. Reagent addition ratios witnessed to complement the various stages of processing are within expected addition rates indicating that operational costs will be on the lower side given these consumption rates.

The overall program was conducted over a 4-month period which consisted of detailed material multi-element analysis, followed by an initial laboratory testwork phase that was conducted 'at lab scale' to ensure the conversion parameters were set for the pilot run, with the pilot program consisting of 2 x 300kg runs thought to the production of Li2SO4.

Raw Material Analysis

Analysis was conducted on the spodumene concentrate delivered to EcoPro's Pohang laboratory and technical production in bulk bags transported by ship from Thunder Bay. It was pretreated using a microwave (Anton Paar, Microwave 5000) and then completely dissolved spodumene was analysed for its components using ICP (PerkinElmer, Avio 500). It was confirmed that the concentrate contains 2.76 % of Li (5.95 % as Li_2O), with major impurities being 1.93 % of Ca and 1.47% of K. The Si element in the concentrate was excluded from the analysis results due to volatilisation during pretreatment with hydrofluoric acid (HF).

Element	Na	Ca	Mg	Fe	Cr	Zn	K	Ni	Co	Mn	Al	Li	Pb	Cu	Ti	S	B
Content (%)	0.98	1.93	0.10	0.41	0.10	0.04	1.47	0.005	0.002	0.29	11.98	**2.76**	0.01	0.005	0.01	0.02	0.003

Table 2: Composition Analysis Results of Spodumene Concentrate

Particle size distribution analysis of spodumene concentrate was conducted through sieving, and the results confirmed that most particles are composed of sizes ranging from 1 to 9.5 mm.

Size	9.5 mm ↑	4.0 mm ↑	2.0 mm ↑	1.0 mm ↑	0.6 mm ↑	0.6 mm ↓
Content	0 %	33.5 %	42.1 %	21.6 %	2.2 %	0.6 %

Table 3. Particle Size Distribution of Spodumene Concentrate (Sieving Analysis)

Flow Sheet and test work summary

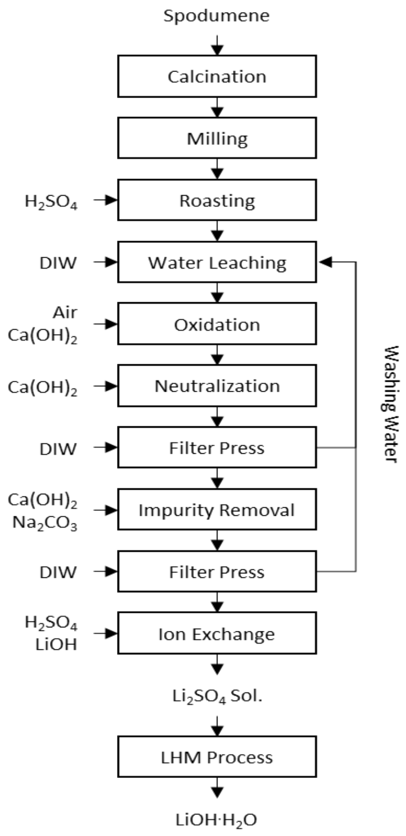

Figure 1. Flow Sheet for Manufacturing Lithium Hydroxide Monohydrate from Spodumene

The process used for the testwork to produce lithium hydroxide monohydrate from spodumene concentrate consists of Calcination, Sulfuric Acid Roasting, Leaching, Oxidation, Neutralisation, Impurity Removal, Ion Exchange, and final lithium hydroxide production stages, as shown in Figure 1. The process is known as the 'standard' spodumene to lithium hydroxide flowsheet and is similar in nature to multiple operations globally that successfully currently produce commercial scale product sold into the battery materials market and is the preferred technical solution employed by EcoPro for spodumene conversion and processing.

First, the calcination process was performed to thermally treat α-spodumene and convert it to β-spodumene, a structure that facilitates lithium extraction. Subsequently, sulfuric acid is added to convert $LiAlSi_2O_6$ in β-spodumene to $HAlSi_2O_6$ and Li_2SO_4 through sulfuric acid roasting process. The generated lithium sulfate (Li_2SO_4) has high solubility in water, making it easy to recover in aqueous through simple leaching.

After leaching, oxidation and neutralisation processes were carried out to remove impurities such as Fe, Cr, Zn and Mn present in the spodumene concentrate. After adding the neutralising agent, solid-liquid separation was performed to separate the lithium sulfate solution from the neutralisation residue. To improve lithium recovery, additional washing water was then added and recycled back into the leaching process.

Subsequently, calcium hydroxide ($Ca(OH)_2$) and sodium carbonate (Na_2CO_3) added to remove Ca and Mg from the solution, and ion exchange process performed to reduce the calcium concentration in the filtrate to below 1 mg/kg. Finally, the purified lithium sulfate solution was used to produce battery-grade lithium hydroxide monohydrate ($LiOH.H_2O$) using EcoPro Innovation's LHM process.

Initial Testwork

Initial testwork was completed to set test conditions for the pilot scale work, with successful results produced from optimal laboratory conditions. Importantly results of calcination on Seymour concentrates conducted previously by the company with pyrometallurgical specialists FLS at their North American facilities rendered similar results.

Calcination & Sulfuric Acid Roast Testing

To convert α-spodumene to β-spodumene, which facilitates lithium extraction, calcination was performed using EcoPro's pilot scale roasting kiln. The calcination temperature was adjusted from 900 °C to 1,100 °C, with the calcination time fixed, to determine the optimal conditions. To evaluate the optimal conditions for each calcination temperature, the lithium recovery rate was assessed through subsequent sulfuric acid roasting and leaching processes. The sulfuric acid roasting process was carried out at 250 °C for with 1.4 equivalents of sulfuric acid relative to the lithium in the concentrate

Results showed that when the calcination temperature was above 1,000 °C, the lithium recovery rates exceeded 97 %. XRD analysis confirmed that α-spodumene was converted to β-spodumene at temperatures above 950 °C. In the case of other companies' concentrates, the phase transformation to β-spodumene was observed at temperatures above 1,000 °C, and lithium recovery was achieved at temperatures above 1,050 °C. The spodumene concentrate used in this experiment contained 1.93% of Ca, which is higher than other concentrates. According to EcpPro Innovation's existing results, the presence of calcium oxide (CaO) in the spodumene concentrate allows for calcination at lower temperatures. Therefore, the high calcium content in this spodumene concentrate likely helps lower the phase transformation and calcination temperatures.

Temperature	900 °C	950 °C	1,000 °C	1,050 °C	1,100 °C
Li Recovery	61.0 %	87.9 %	97.3 %	97.4 %	96.7 %

Table 4. Lithium Recovery Rate by Calcination Temperature

Figure 2: Before (left) and After (right) Sulfuric Acid Roasting After Mixing with Sulfuric Acid

The experimental results showed that when more than 1.2 equivalents of sulfuric acid were added relative to the lithium content in the concentrate at calcination temperatures above 1,000 ℃, the lithium recovery rate exceeded 97 %, which indicates industry leading lab scale recoveries.

H_2SO_4 equivalent Temperature	1.1 eq.	1.2 eq.	1.3 eq.	1.4 eq.	1.5 eq.
950 ℃	85.3 %	89.4 %	88.8 %	90.3 %	88.6 %
1,000 ℃	97.0 %	97.7 %	97.7 %	97.8 %	97.6 %
1,050 ℃	96.2 %	97.4 %	97.6 %	97.5 %	97.7 %

Table 5. Lithium Recovery Rate by Sulfuric Acid Addition at Different Calcination Temperature

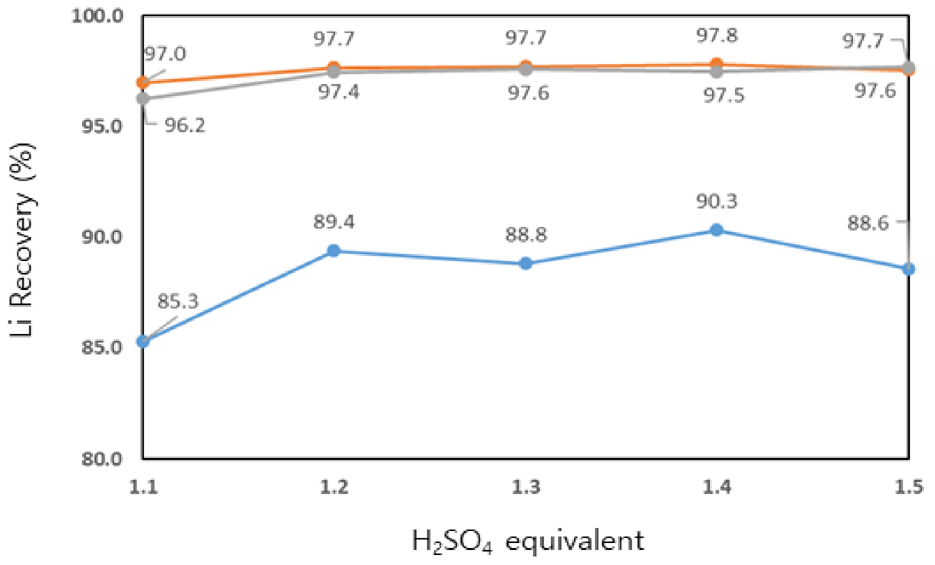

Figure 3: Lithium Recovery Rate by Sulfuric Acid Addition at Different Calcination Temperatures (as depicted in Table 5)

To verify the reproducibility of the sulfuric acid addition, sulfuric acid roasting experiments were performed at 250 ℃ with 1.2 equivalents of sulfuric acid relative to the lithium content in the spodumene concentrate at different calcination temperatures. The leaching conditions were maintained the same as before, with a solid-liquid ratio of 40 %. The reproducibility experiments confirmed that the lithium recovery rate remained above 97% when calcination temperatures were between 1,000 ℃ and 1,050 ℃, using 1.2 equivalents of sulfuric acid.

Temperature	**900 ℃**	**950 ℃**	**1,000 ℃**	**1,050 ℃**	**1,100 ℃**
Li Recovery	57.4 %	92.8 %	97.7 %	97.4 %	95.4 %

Table 6. Lithium Recovery Rate by Sulfuric Acid Roasting at Different Calcination Temperatures

Therefore, the optimal conditions for the calcination process were determined to be 1,000 ℃, and the optimal conditions for the sulfuric acid roasting process were determined to be 250 ℃ with 1.2 equivalents of sulfuric acid relative to the lithium content in the spodumene concentrate. The lithium concentration in the leachate from the leaching process performed under these conditions is shown in Table 7.

Element	**Na**	**Ca**	**Mg**	**Fe**	**Cr**	**Zn**	**K**	**Si**	**Ni**	**Co**	**Mn**	**Al**	**Li**	**S**
(mg/kg)	354	460	18	43	0	26	208	54	0	0	525	102	**12,103**	28,066

Table 7: Leachate Concentration Under Optimal Calcination-Sulfuric Acid Roasting Conditions

Leaching, Oxidation and Neutralisation Test

To effectively remove impurities (Fe, Zn, Mn, Al, etc.) generated during the leaching process, the oxidation and neutralisation process was conducted. Instead of performing solid-liquid separation immediately after leaching process, it was carried out after neutralisation process to reduce process steps and improve separation speed.

The results of the leaching, oxidation and neutralisation processes confirmed that most impurities were removed, with an average lithium recovery rate of 95.7%. Although there were some prior concerns about the leaching of a large amount of potassium due to the potassium content of 1.47 % in the spodumene concentrate, careful monitoring of this aspect demonstrated that the potassium content in the neutralisation filtrate was found to be at a readily acceptable level of only about 300 mg/kg.

Although the spodumene concentrate contains a large amount of K, it exists in the form of K-Al-Si compounds of the feldspar series rather than being leached in combination with lithium, so only minor amount of K was leached, and the majority was removed easily within the insoluble residue.

Impurity Removal (Ca, Mg) Test

To remove residual impurities (Ca, Mg) in the filtrate after the neutralisation process, the impurity removal process was conducted. This process involved adjusting the pH using a calcium hydroxide slurry at to first remove Mg, followed by the addition of sodium carbonate in the filtrate to remove Ca. The goal of this process was to reduce Mg to less than 1 mg/kg and Ca to less than 30 mg/kg. The main reactions are as follows:

1) $MgSO_4 + Ca(OH)_2 \rightarrow Mg(OH)_2(\downarrow) + CaSO_4$
2) $CaSO_4 + Na_2CO_3 \rightarrow CaCO_3(\downarrow) + Na_2SO_4$

The impurity removal results confirmed that Ca was reduced to 28 mg/kg and Mg to 0 mg/kg, meeting the target criteria. It was also confirmed that the small amount of Mn remaining after the neutralisation process was completely removed.

Element Process	Na	Ca	Mg	K	Si	Ni	Co	Mn	Al	Li	S
Neutralisation	672	491	59	274	15	0	0	5	0	**14,462**	28,066
Impurity removal	2,307	28	0	284	11	0	0	0	0	**15,421**	31,094

Table. 8. Analysis Results of Filtrate from Neutralisation and Impurity Removal Processes

Reproducibility Verification of Calcination to Impurity Removal Process

The reproducibility tests were conducted over a total of 4 cycles to verify the reproducibility of the calcination process to the impurity removal process. In the leaching, oxidation and neutralisation process, the cake washing filtrate generated during the solid-liquid separation step after neutralisation process was recycled into the leaching solution to increase the lithium concentration in the filtrate. This test was conducted based on the optimal conditions derived from previous lab. Tests.

The reproducibility test from calcination process to the neutralisation process confirmed that the average lithium recovery rate was 95.4%, similar to the lab. test results. Additionally, by recycling the cake washing filtrate generated during the solid-liquid separation step after neutralisation process into the leaching solution, it was confirmed that the lithium concentration increased from 12.0 g/kg to 13.5 g/kg. As the number of cycles increased, the lithium concentration also increased proportionally, but it converged after a certain point, indicating that the lithium concentration level of 16~20 g/kg is applicable to the LHM Process of EcoPro Innovation.

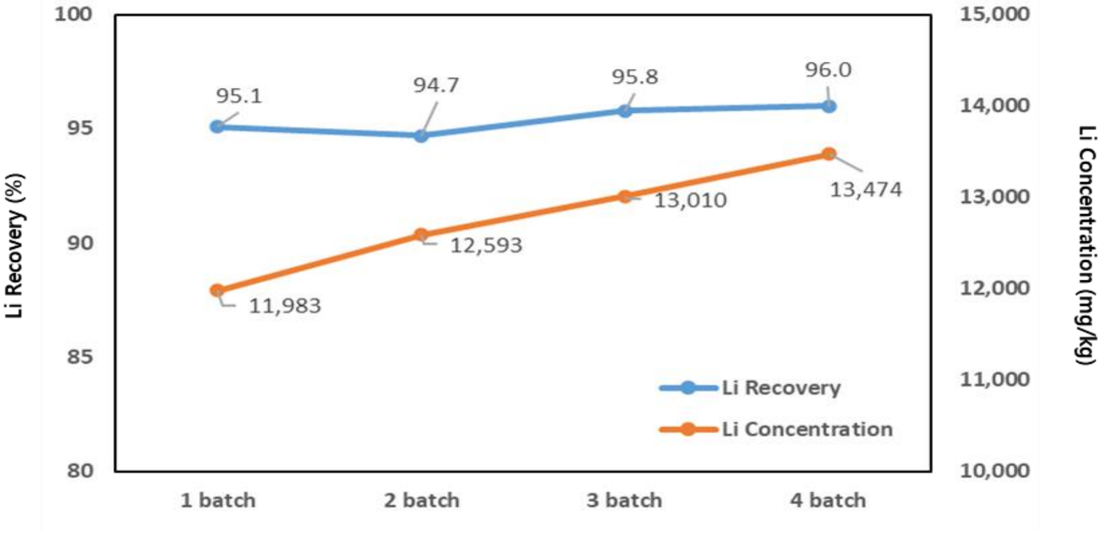

Figure 4: Lithium Recovery Rate and Concentration in Reproducibility test from Calcination Process to Neutralisation Process

The reproducibility tests for the impurity removal process using the filtrate from the calcination to neutralisation process confirmed that Ca was reduced to less than 15 mg/kg and Mg to less than 1 mg/kg in all 4 cycles, similar to the lab. test results.

Due to the large amount of solution required, the ion exchange process and LHM process, which are subsequent to impurity removal process, were not conducted using the lab. test filtrate but were instead conducted using the pilot test filtrate. The results of these processes are documented in the pilot scale testing section below.

Pilot Scale testing

Based on the results of the spodumene concentrate lab tests, a pilot scale test was conducted using pre-established pilot plant equipment to cover the entire process from calcination to lithium hydroxide production process. This test aimed to verify the continuity, reproducibility, and lithium recovery rate of the process using actual equipment, based on the optimal conditions secured at the lab. test.

The main equipment used in the pilot test includes:

- Rotary Kiln: Calcination and sulfuric acid roasting of spodumene concentrate
- Cutter Mill: Primary crushing for particle size adjustment after calcination process
- Hammer Mill: Additional fine crushing process
- Reactor: Leaching, oxidation, neutralisation and impurity removal reaction process

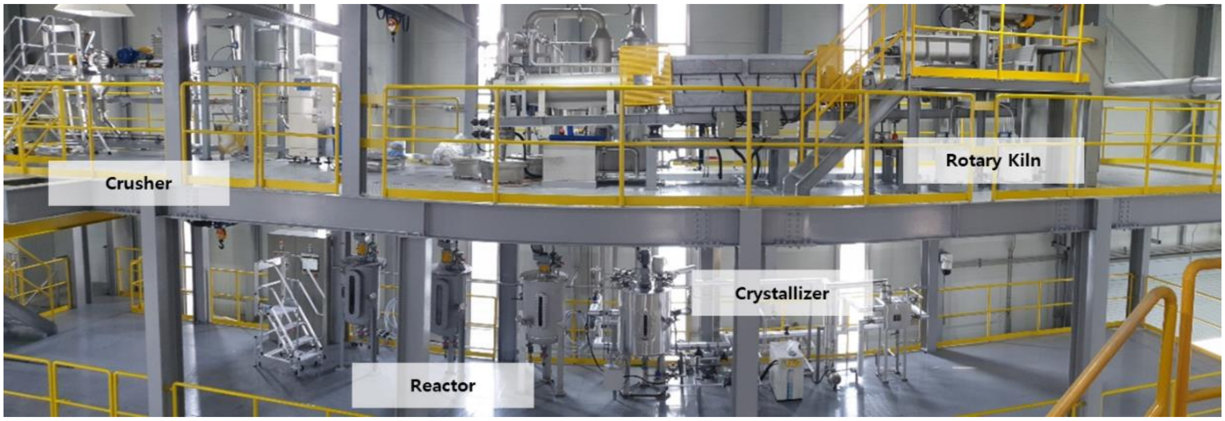

Figure 5: Pilot Test Equipment

Calcination Test

A total of 600 kg of spodumene concentrate was calcined in two batches of 300 kg each using a rotary kiln at 1,050 °C without particle size adjustment. The feed rate was 10 kg per hour. Although the optimal calcination temperature derived from the lab test was 1,000 °C, the temperature was adjusted to 1,050 °C considering the internal heat transfer rate and operating conditions of the pilot scale rotary kiln.

Figure 6: Rotary Kiln (left) and Calcination Test (right)

After sampling the calcined material at different operating times of the rotary kiln, sulfuric acid roasting and leaching test were conducted in the lab. for each sample. This test applied the same sulfuric acid roasting and leaching process conditions as the optimal conditions derived from the lab. test to evaluate the efficiency of the pilot scale calcination process.

The test results showed lithium recovery rates of 96.7 % and 97.7 %, with an average recovery rate of 97.2 % for the total 600 kg. This indicates that the calcination performance at the pilot scale is comparable to the laboratory scale test results, with a lithium recovery rate of 97.7 % in the lab calcination test.

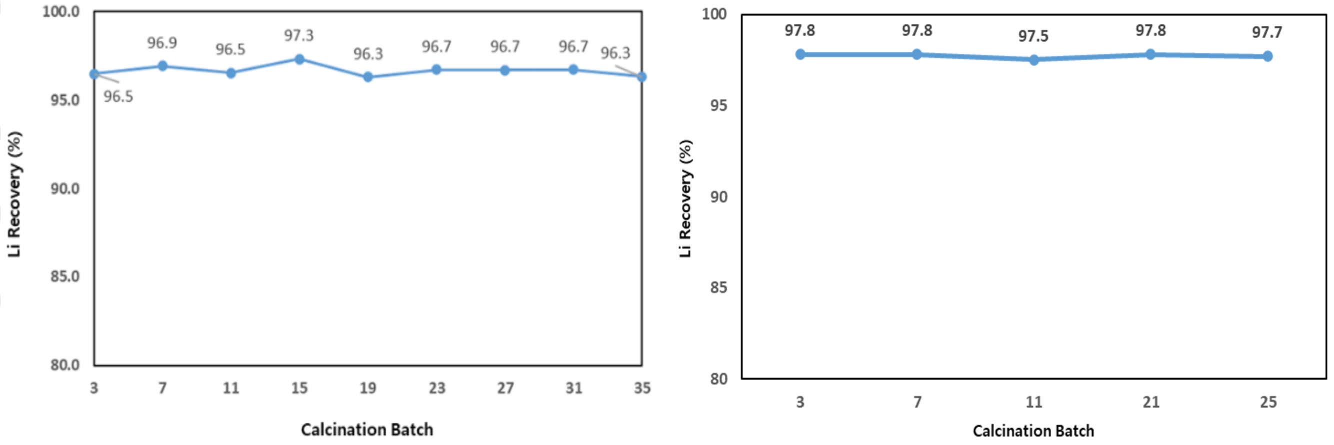

Figure 7: Lithium Recovery Rate in Calcination Process of Pilot Test (left : 1 batch, right : 2 batch)

Crushing and Sulfuric Acid Roasting Test

After calcination process, particle size distribution analysis was conducted on the spodumene concentrate samples through sieving, revealing that 48.8 % of the particles were larger than 1 mm. This confirmed the necessity of a crushing process before the sulfuric acid roasting process. Consequently, particle size adjustment was performed sequentially using a cutter mill and a hammer mill.

Using samples crushed with the hammer mill, sulfuric acid roasting tests were conducted in the rotary kiln. The test were carried out continuously, with sulfuric acid added at 1.3 equivalents relative to the lithium content in the spodumene concentrate. Although the optimal conditions for sulfuric acid roasting derived from the lab. test were lower, the conditions were adjusted upward considering the internal heat transfer rate of the rotary kiln, similar to the calcination process.

Figure 8: Adhesion Inside Rotary Kiln During Sulfuric Acid Roasting of Hammer Mill Crushed Samples(left) and Cutter Mill Crushed Samples After Sulfuric Acid Roasting

Using 350 kg of cutter mill crushed samples, sulfuric acid roasting test were conducted in the rotary kiln in two batches. The test conditions were the same as those for the hammer mill crushed samples, with continuous operation in line with the previous testwork with sulfuric acid equivalents added relative to the lithium content in the spodumene concentrate. After sulfuric acid roasting, sampling was conducted at intervals, and leaching test were performed in the lab. for each sample to evaluate the efficiency of the pilot scale sulfuric acid roasting process. The leaching test applied the same optimal conditions derived from the lab. test.

The results of the pilot scale sulfuric acid roasting test showed lithium recovery rates of 96.3% and 96.6%, with an average recovery rate of 96.5% for the total 350 kg. This indicates that the sulfuric acid roasting performance at the pilot scale is comparable to the laboratory Scale results, with a lithium recovery rate of 97.7% in the lab sulfuric acid roasting test.

Leaching, Oxidation and Neutralisation Test

A series of tests were conducted on the samples generated after sulfuric acid roasting, including leaching, oxidation and neutralisation processes. These processes were carried out at a standard reaction temperature, with leaching performed at acceptable solid-liquid ratios. In the oxidation process, the pH was adjusted with calcium hydroxide slurry, and air was injected to induce the reaction. In the subsequent neutralisation process, the pH was adjusted using the same concentration of calcium hydroxide slurry, maintained for, and then solid-liquid separation was performed to complete the final treatment.

Figure 9: Reaction Reactor (left), Residue (right)

The leaching, oxidation and neutralisation processes were repeated five times, and the results showed that the lithium concentration in the filtrate was 13.2 g/kg, with major impurities including Ca 397 mg/kg, Mg 35 mg/kg and Mn 33 mg/kg. These impurities can be effectively removed through subsequent impurity removal and ion exchange processes, which was similar to the results obtained in previous lab. tests.

The average lithium recovery rate for the leaching, oxidation and neutralisation processes was 92.7 %, which is slightly lower than the 95.7 % achieved under optimal conditions in the lab. test. This difference is attributed to the use of a filter press during the solid-liquid separation process, where the low washing efficiency of the filter press resulted in some lithium being lost with the cake, leading to a decrease in recovery rate. In future mass production processes, it is expected that the recovery rate can be improved by using a belt filter instead of a filter press to enhance washing efficiency.

Impurity removal test

To remove residual impurities (Ca, Mg) in the filtrate after the neutralisation process, the impurity removal process was conducted. This process involved adjusting the pH using a calcium hydroxide slurry to first remove Mg, followed by the addition of sodium carbonate at 2 equivalents relative to the calcium content in the filtrate to remove Ca.

Figure 10: Impurity Removal Process Equipment

The impurities remaining in the filtrate after neutralisation process, Ca 397 mg/kg, Mg 35 mg/kg, Mn 33 mg/kg, were reduced to Ca 16 mg/kg, Mg and Mn 0 mg/kg through the impurity removal process, reaching the target values. These results are similar to the results obtained in previous lab. tests.

Ion Exchange Test

To reduce the calcium content in the filtrate from 16 mg/kg to less than 1 mg/kg after impurity removal, ion exchange processing was conducted.

The ion exchange process used known resins for cation adsorption. For the regeneration and conversion process of the resin, HCl and LiOH solutions were applied, which is a differentiated approach compared to the NaOH based conversion conditions proposed by Lanxess. By using LiOH instead of NaOH, the solution generated after conversion could be recycled in to the water leaching process instead of wastewater treatment, allowing for additional recovery of residual lithium in the filtrate.

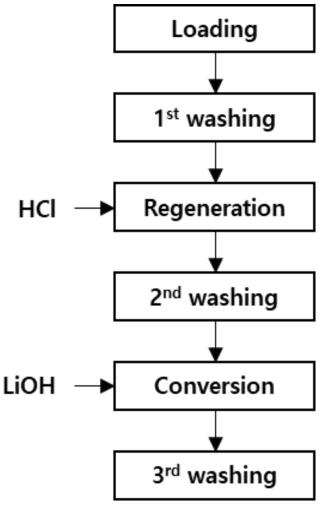

Figure 11: Flow Sheet of Ion Exchange Process

After Bed Volumes (BV) treatment in the ion exchange process, an increase in Ca concentration exceeding 1 mg/kg in the filtrate was observed, with the amount of Ca adsorbed on the resin, similar to the standard proposed by Lanxess.

Lithium Hydroxide Monohydrate Production Test

This test was conducted based on the lithium hydroxide monohydrate production process currently operated by EcoPro Innovation, using lithium sulfate solution produced through the ion exchange process as the raw material. To convert lithium sulfate to lithium hydroxide, NaOH was added, and $Na_2SO_4 \cdot 10H_2O$ and lithium hydroxide were separated through a cooling separation process utilising solubility differences. Subsequently, impurities were controlled through crystallisation and re-dissolution process, and finally, lithium hydroxide monohydrate was produced.

Figure 12: Cooling Separation Test (left) and Crystallisation Test (right)

The XRD analysis of the produced lithium hydroxide showed no impurity peaks other than lithium hydroxide monohydrate, and titration and ICP analysis confirmed it to be 56.5% of lithium hydroxide. Additionally, impurity analysis revealed the presence of 4,889 mg/kg of Li2CO3, 14 mg/kg of Na, and 9 mg/kg of S. This confirms the feasibility of producing battery-grade lithium hydroxide monohydrate using spodumene concentrate.

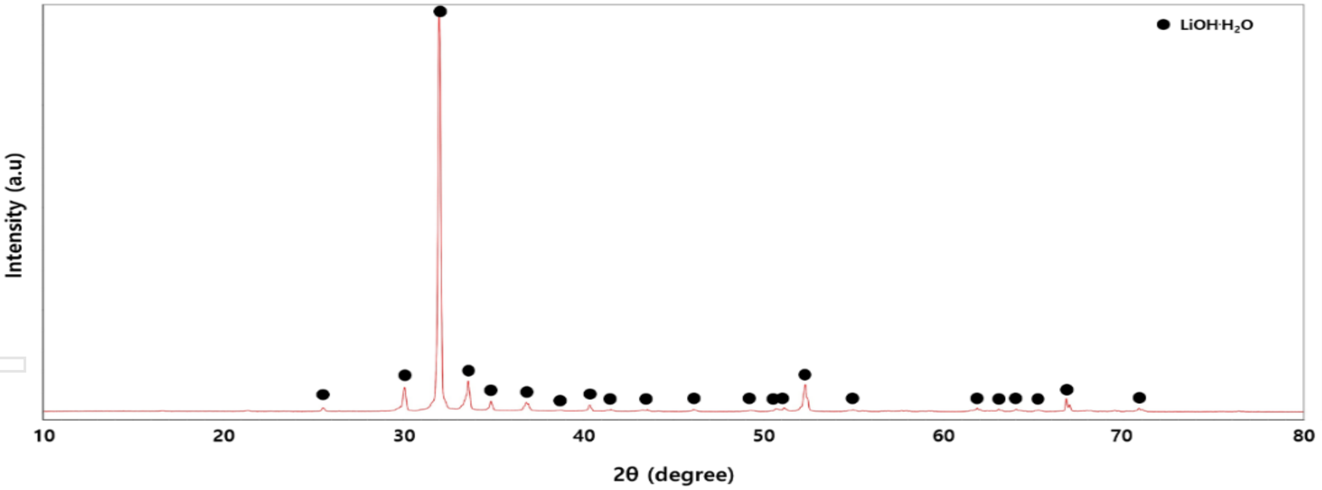

Fig 13: XRD Analysis Results of Lithium Hydroxide Monohydrate

Further work

Based on the successful testwork and piloting program various follow-up work will continue at EcoPro's testing facility to further optimise operating conditions, reagent addition and product definition. The parameters defined throughout the programs will all feed into process design criteria's currently being developed for scale-up plant design within the proposed Thunder Bay conversion facility in which both GT1 and EcoPro may enter into a joint venture to develop post the completion of the PFS which is currently underway.

Given the Root bulk sample has already been taken the next phases will also include piloting work to produce a 5.5% Li2O concentrate for a second pilot program at EcoPro's facility to confirm the Root projects concentrates can also be readily converted.

Indigenous Partner Acknowledgement

We would like to say Gchi Miigwech to our Indigenous partners. GT1 appreciates the opportunity to work in the Traditional Territory and remains committed to the recognition and respect of those who have lived, travelled, and gathered on the lands since time immemorial. Green Technology Metals is committed to stewarding Indigenous heritage and remains committed to building, fostering, and encouraging a respectful relationship with Indigenous Peoples based upon principles of mutual trust, respect, reciprocity, and collaboration in the spirit of reconciliation.

KEY CONTACTS

This announcement was authorised for release by the Board of Directors

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Green Technology Metals (ASX:GT1)

GT1 is a North American-focussed lithium exploration and development business with a current global Mineral Resource estimate of 30.4Mt at 1.17% Li_2O.

Project	Tonnes (Mt)	Li_2O (%)
Root Project		
Root Bay Open pit		
Indicated	5.8	1.28
Inferred	0.1	0.73
Root Bay Underground		
Indicated	4.2	1.37
Inferred	5.5	1.24
McCombe		
Inferred	4.5	1.01
Root Total	**20.1**	**1.24**

Seymour Project[1]		
North Aubry		
Indicated	6.1	1.25
Inferred	2.1	0.8
South Aubry		
Inferred	2.0	0.6
Seymour Total	**10.3**	**1.07**
Combined Total	**30.4**	**1.17**

The Company's main 100% owned Ontario lithium projects comprise high-grade, hard rock spodumene assets (Seymour, Root, Junior and Wisa) and lithium exploration claims (Allison, Falcon, Gathering, Pennock and Superb) located on highly prospective Archean Greenstone tenure in north-west Ontario, Canada. All sites are proximate to excellent existing infrastructure (including clean hydro power generation and transmission facilities), readily accessible by road, and with nearby rail delivering transport optionality. Targeted exploration across all three projects delivers outstanding potential to grow resources rapidly and substantially.

[1] For full details of the Seymour Mineral Resource estimate, see GT1 ASX release dated 21 November 2023, *Seymour Resource Confidence Increased - Amended*. For full details of the Root Mineral Resource estimate, see GT1 ASX release 18 October 2023, *Significant resource and confidence level increase at Root, Global Resource Inventory now at 24.5Mt*. The Company confirms that it is not aware of any new information or data that materially affects the information in that release and that the material assumptions and technical parameters underpinning this estimate continue to apply and have not materially changed.

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[1] For full details of the Seymour Mineral Resource estimate, see GT1 ASX release dated 21 November 2023, Seymour Resource Confidence Increased-Amended.

APPENDIX A: IMPORTANT NOTICES

Competent Person's Statement

The information in this report relating to Metallurgical results is based on information reviewed by the Company's Non-Executive Chairman, Mr John Young, a competent person, who is a Member of the Australian Institute of Mining and Metallurgy. Mr Young has sufficient experience relevant to the style of mineralisation and to the type of activity described to qualify as a competent person as defined in the 2012 Edition of the "Australasian Code for Reporting of Exploration Results, Mineral Resources and Ore Reserves." Mr Young has disclosed that he holds Shares, Options and Performance Rights in the Company. Mr Young consents to the inclusion in this announcement of the matters based on his information in the form and content in which it appears.

No new information

Except where explicitly stated, this announcement contains references to prior exploration results, all of which have been cross-referenced to previous market announcements made by the Company. The Company confirms that it is not aware of any new information or data that materially affects the information included in the relevant market announcements.

The information in this report relating to the Mineral Resource estimate for the Seymour Project is extracted from the Company's ASX announcement dated 21 November 2023 and 24 July 2025. GT1 confirms that it is not aware of any new information or data that materially affects the information included in the original announcement and that all material assumptions and technical parameters underpinning the Mineral Resource estimate continue to apply.

The information in this report relating to the Mineral Resource estimate for the Root Project is extracted from the Company's ASX announcement dated 3 April 2025. GT1 confirms that it is not aware of any new information or data that materially affects the information included in the original announcement and that all material assumptions and technical parameters underpinning the Mineral Resource estimate continue to apply.

Forward Looking Statements

Certain information in this document refers to the intentions of Green Technology Metals Limited (ASX: GT1), however these are not intended to be forecasts, forward looking statements or statements about the future matters for the purposes of the Corporations Act or any other applicable law. Statements regarding plans with respect to GT1's projects are forward looking statements and can generally be identified by the use of words such as 'project', 'foresee', 'plan', 'expect', 'aim', 'intend', 'anticipate', 'believe', 'estimate', 'may', 'should', 'will' or similar expressions. There can be no assurance that the GT1's plans for its projects will proceed as expected and there can be no assurance of future events which are subject to risk, uncertainties and other actions that may cause GT1's actual results, performance or achievements to differ from those referred to in this document. While the information contained in this document has been prepared in good faith, there can be given no assurance or guarantee that the occurrence of these events referred to in the document will occur as contemplated. Accordingly, to the maximum extent permitted by law, GT1 and any of its affiliates and their directors, officers, employees, agents and advisors disclaim any liability whether direct or indirect, express or limited, contractual, tortuous, statutory or otherwise, in respect of, the accuracy, reliability or completeness of the information in this document, or likelihood of fulfilment of any forward-looking statement or any event or results expressed or implied in any forward-looking statement; and do not make any representation or warranty, express or implied, as to the accuracy, reliability or completeness of the information in this document, or likelihood of fulfilment of any forward-looking statement or any event or results expressed or implied in any forward-looking statement; and disclaim all responsibility and liability for these forward-looking statements (including, without limitation, liability for negligence).

APPENDIX A: JORC CODE, 2012 EDITION – Table 1 Report

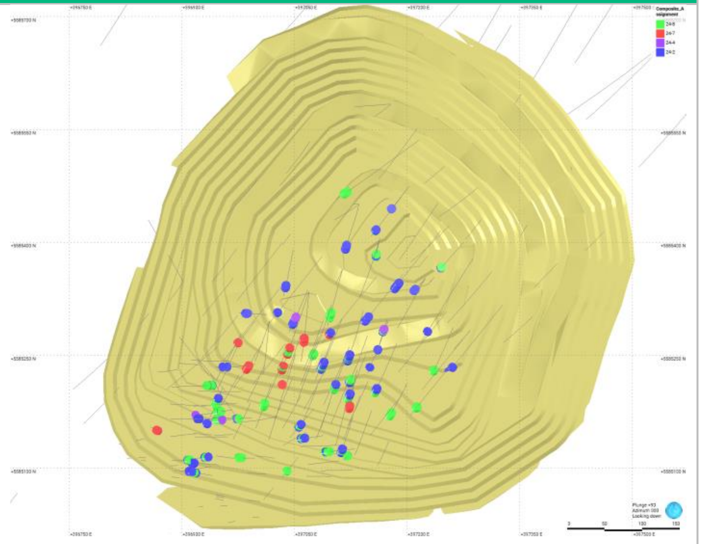
JORC Code, 2012 Edition – Table 1 report template

Section 1 Sampling Techniques and Data

Criteria	JORC Code explanation	Commentary
Sampling techniques	▪ *Nature and quality of sampling (eg cut channels, random chips, or specific specialised industry standard measurement tools appropriate to the minerals under investigation, such as down hole gamma sondes, or handheld XRF instruments, etc). These examples should not be taken as limiting the broad meaning of sampling.* ▪ *Include reference to measures taken to ensure sample representivity and the appropriate calibration of any measurement tools or systems used.* ▪ *Aspects of the determination of mineralisation that are Material to the Public Report.* ▪ *In cases where 'industry standard' work has been done this would be relatively simple (eg 'reverse circulation drilling was used to obtain 1 m samples from which 3 kg was pulverised to produce a 30 g charge for fire assay'). In other cases more explanation may be required, such as where there is coarse gold that has inherent sampling problems. Unusual commodities or mineralisation types (eg submarine nodules) may warrant disclosure of detailed information.*	**No drilling is reported in this release.** **Metallurgy** Metallurgical samples (24-2, 24-4, 24-7 and 24-8) were extracted from the North Aubry deposit within a USD2500 pit design from 65 historic and GT1 drill hole ¼ diamond core reserves for 655m. Drilling methodology aligned with previous drilling practices which are considered standard. Head assays were back calculated post testing and compared with the head sample submitted, with the lithium and iron grades within suitable tolerance. **Ore Sorting** Ore Sorting samples were obtained as follows: (i) samples from two composites 24-2 and 24-4 prepared as outlined above, and (ii) samples for two composites 24-5 and 24-6 that were extracted from material obtained from trench sampling, which is considered suitable for representative bulk sample testwork. The trenches (Trench Ids: GTTR-23-01, GTTR-23-10, GTTR-23-11, GTTR-23-12) were located within the mine pit shell where the primary outcrop existed, and incorporated sufficient host rock for dilution impacts to be investigated. Over 80 tonne was collected from which two 700kg composites were generated, on a weighted for size distribution based on the crushing model. The 4 composites above were prepared by SGS Lakefield for Ore Sorting with a coarse (-9/+3") and a fine (-3/+1") fraction for each. Head assays were back calculated post testing and compared with the head sample submitted, generally the lithium grade was within tolerance, the iron grades had some variability due to the coarse material size and the significant variability between the ore and host material. The -1" fraction was then removed and retained at SGS, whilst the ore sorting samples were sent to Steinert USA. The samples were scanned by Steinert using a combination sensor sorter testing different sorting techniques, with laser and XRT proving the most effective. Li_2O product grades increased, and iron grades reduced in line with ore sorter upgrade and mass rejection predictions and aligned with dilution ratios applied. Bulk Sampling Bulk sample collected by GT1 follows industry standard practices, including dice pattern drill holes at tight spacing (<1m) to ensure liberation of minerals and small particle size of material (<30cm, nominally 15cm). Blast area was covered with clean rubber blast mats to ensure material is liberated but not ejected from sample site. Three blasts were conducted along the path of channel samples collected by the company to correlate Lithium grade on surface to that of the blasted material. The resulting pit is 1m deep and a number of metres wide/long and was designed to stay under the 100tonne threshold of the permit acquired to complete the work. The resulting material displayed the extremely coarse nature of the North Aubry deposit, with spodumene crystals over 30cm in length extremely common. The bulk sample was collected at 396,950.29E 5,585,061.32N m (UTM

Criteria	JORC Code explanation	Commentary
		NAD83 Z16) and material was placed into 1m3 bulk bags and shipped from site on flatbed trailers. The bulk sample also included 4tonnes of host or country rock to be available for ore dilution studies.
Drilling techniques	- *Drill type (eg core, reverse circulation, open-hole hammer, rotary air blast, auger, Bangka, sonic, etc) and details (eg core diameter, triple or standard tube, depth of diamond tails, face-sampling bit or other type, whether core is oriented and if so, by what method, etc).*	**No drilling is reported in this release.**
Drill sample recovery	- *Method of recording and assessing core and chip sample recoveries and results assessed.* - *Measures taken to maximise sample recovery and ensure representative nature of the samples.* - *Whether a relationship exists between sample recovery and grade and whether sample bias may have occurred due to preferential loss/gain of fine/coarse material.*	**No drilling is reported in this release.**
Logging	- *Whether core and chip samples have been geologically and geotechnically logged to a level of detail to support appropriate Mineral Resource estimation, mining studies and metallurgical studies.* - *Whether logging is qualitative or quantitative in nature. Core (or costean, channel, etc) photography.* - *The total length and percentage of the relevant intersections logged.*	**No drilling is reported in this release.**
Sub-sampling techniques and sample preparation	- *If core, whether cut or sawn and whether quarter, half or all core taken.* - *If non-core, whether riffled, tube sampled, rotary split, etc and whether sampled wet or dry.* - *For all sample types, the nature, quality and appropriateness of the sample preparation technique.* - *Quality control procedures adopted for all sub-sampling stages to maximise representivity of samples.* - *Measures taken to ensure that the sampling is representative of the in situ material collected, including for instance results for field duplicate/second-half sampling.* - *Whether sample sizes are appropriate to the grain size of the material being sampled.*	**No drilling is reported in this release.**
Quality of assay data and laboratory tests	- *The nature, quality and appropriateness of the assaying and laboratory procedures used and whether the technique is considered partial or total.* - *For geophysical tools, spectrometers, handheld XRF instruments, etc, the parameters used in determining the analysis including instrument make and model, reading times, calibrations factors applied and their derivation, etc.* - *Nature of quality control procedures adopted (eg standards, blanks, duplicates, external laboratory checks) and whether acceptable levels of accuracy (ie lack of bias) and precision have been established.*	For Conversion Testwork - Laboratory and pilot tests were conducted at EcoPro Innovation facilities in Pohang, South Korea. The company has relied upon EcoPro Innovation internal testing and calibration procedures that are tested and proven from commercial operation and the sale of Lithium Hydroxide under commercial conditions with stringent specifications. - All protocols employed are deemed appropriate for the sampling and testing for the conversion of spodumene concentrate to lithium hydroxide. All procedures are considered appropriate for sample type and nature of mineralization and are considered an optimal approach for maintaining representativeness in sampling. For bulk sample concentration metallurgical testwork: - Test work program was conducted at SGS Lakefield Laboratories Ltd, a reputable mineral processing laboratory, who has stringent analytical structures. - Analytical reconciliation for tests were with acceptable tolerances for the material tested.

Criteria	JORC Code explanation	Commentary
Verification of sampling and assaying	▪ *The verification of significant intersections by either independent or alternative company personnel.* ▪ *The use of twinned holes.* ▪ *Documentation of primary data, data entry procedures, data verification, data storage (physical and electronic) protocols.* ▪ *Discuss any adjustment to assay data.*	▪ The majority of laboratory assay results have been sourced directly from the laboratory and the laboratory file directly imported into GT1's SQL database. ▪ All recent north seeking gyroscope surveys are uploaded directly from the survey tool output file and visually validated. ▪ Geological logs and supporting data are uploaded directly to the database using custom built importers to ensure no chance of typographical errors. ▪ No adjustment to laboratory assay data was made. ▪ Assaying of channel samples located on the bulk sample outcrop was completed prior to blasting and are contained in the company's geochemical database
Location of data points	▪ *Accuracy and quality of surveys used to locate drill holes (collar and down-hole surveys), trenches, mine workings and other locations used in Mineral Resource estimation.* ▪ *Specification of the grid system used.* ▪ *Quality and adequacy of topographic control.*	▪ A GPS reading was taken for each sample location using UTM NAD83 Zone16 (for Seymour); waypoint averaging or dGPS was performed when possible. ▪ The project area was flown using LIDAR equipment in October 2021 by KBM Resources Group Inc. from Thunder Bay using a Riegl 680i LiDAR system, coupled to a Applanix POSAV 510 positioning system. The topographic mapping produced is extremely accurate and well suited for resource modelling. ▪ All drilling collars coordinates were compared to the Lidar elevation data to ensure no erroneous coordinates were present in the database. Some collar RL's were adjusted to the Lidar elevation where they differed by more than 3m. GT1 employed a calibrated Reflex SprintIQ North Seeking Gyroscopic tool on all 2021 and 2022 drill holes and surveyed the holes in their entirety with readings downhole every 5m. North Seeking gyroscopes have a typical azimuth accuracy of +/-0.75 degrees and +/-0.15 degrees for dip. ▪ The centroid of the bulk sample blast site is 396,950.29E 5,585,061.32N m (UTM NAD83 Z16) ▪ **Metallurgy** Location of the North Aubry metallurgical samples coloured by assigned ore type within a USD2500 pit design:

Criteria	JORC Code explanation	Commentary
		
Data spacing and distribution	- *Data spacing for reporting of Exploration Results.* - *Whether the data spacing and distribution is sufficient to establish the degree of geological and grade continuity appropriate for the Mineral Resource and Ore Reserve estimation procedure(s) and classifications applied.* - *Whether sample compositing has been applied.*	**Metallurgy** - Prior to bulk sampling, all available historic and more recent GT1 drill core was used to provide metallurgical testwork samples. The samples were distributed roughly on a 50m SE x 100m NW grid with closer spaced shallower samples. - Bulk sampling of the North Aubry deposit was completed at a single location, an exposed outcrop, to earth moving activites and to ensure blasting of representative pegmatite ore. The sample site is 396,950.29E 5,585,061.32N m (UTM NAD83 Z16) -
Orientation of data in relation to geological structure	- *Whether the orientation of sampling achieves unbiased sampling of possible structures and the extent to which this is known, considering the deposit type.* - *If the relationship between the drilling orientation and the orientation of key mineralised structures is considered to have introduced a sampling bias, this should be assessed and reported if material.*	- GT1 drill samples were drilled close to perpendicular to the strike of the pegmatite unit and sampled the entire length of the pegmatite as well including several metres into the mafic country rock either side of the pegmatite. - GT1 North Aubry bulk sample location represents the top of the deposit, that is exposed at surface. No consideration was made with respect to orientation of sample collection, as the orebody is massive in nature.
Sample security	- *The measures taken to ensure sample security.*	- All core and samples were supervised and secured in a locked vehicle, warehouse, or container until delivered to Actlabs in Thunder Bay for cutting, preparation and analysis. - All bulk sample material followed proper chain of custody. Bags were filled, labelled, sealed and loaded onto flatbed trucks on-site and were immediately transported to the contractors gated yard, where they were held for a number of days before shipping to concentrator at SRC Labs in Saskatchewan Canada. **Metallurgy** - Historic and GT1 ½ core was either cut in GT1' s Thunder Bay core storage facility or delivered under GT1 supervision to Diamond Daves', Thunder Bay, a core cutting contractor. Samples were ¼ core cut using a diamond saw and composited into nominally 1m lengths retained in numbered calico bags themselves grouped into labelled poly weave bags for delivery to the metallurgical laboratory.
Audits or reviews	- *The results of any audits or reviews of sampling techniques and data.*	**No drilling is reported in this release.**

Section 2 Reporting of Exploration Results

(Criteria listed in the preceding section also apply to this section.)

Criteria	JORC Code explanation	Commentary
Mineral tenement and land tenure status	- *Type, reference name/number, location and ownership including agreements or material issues with third parties such as joint ventures, partnerships, overriding royalties, native title interests, historical sites, wilderness or national park and environmental settings.* - *The security of the tenure held at the time of reporting along with any known impediments to obtaining a licence to operate in the area.*	- Green Technology Metals (ASX:GT1) owns 100% interest in the Ontario Lithium Projects (Seymour, Junior, Root and Wisa). - Seymour Lithium Asset consists of 660 Cell Claims (Exploration Licences) and one Mining Lease, with a total claim area of 15,140 ha. - GT1 have acquired several additional claims around Seymour, Root, Allison Lake and Landore since listing on the ASX. - As of the effective date of this report, all subject lands are in good standing and all claims are currently held 100% by Green TM Resources (Canada) Ltd (a subsidiary of Green Technology Metals Ltd). - As the claims are on Crown Land, surface access is guaranteed under the Mining Act of Ontario. - All Cell Claims are in good standing - Exploration Agreements are current with the Whitesand First Nation, AZA First Nation, BNA First Nation, and BZA First Nation to support of GT1 exploration activities
Exploration done by other parties	- *Acknowledgment and appraisal of exploration by other parties.*	- Regional exploration for lithium deposits commenced in the 1950's. In 1957, local prospector, Mr Nelson Aubry, discovered the North Aubry and the South Aubry pegmatites. - Geological mapping by the Ontario Department of Mines commenced in 1959 and was completed in 1962 (Pye, 1968), with the publication of "Map 2100 Crescent Lake Area" in 1965. - From the late 1950's to 2002, exploration by the Ontario Department of Mines was generally restricted to geological mapping and surface sampling, although some minor drilling was completed to test the North Aubry pegmatite in late 1957 (Rees, 2011). - In 2001, Linear Resources Inc. ("Linear Resources") obtained the Seymour Lake Project with an initial focus on the project's tantalum potential. In 2002, a 23-diamond drill-hole campaign was completed at North Aubry, and a further 8 diamond drill-holes at South Aubry. - In 2008, Linear Resources completed a regional soil-sampling program which resulted in the identification of a number soil geochemical anomalies. Based on these anomalies, another drilling campaign (completed in 2009), with 12 diamond drill-holes at North Aubry, 2 diamond drill-holes at South Aubry, and further 5 diamond drill-holes peripheral to the Aubry prospects designed to test the main 2008 soil geochemical anomalies. - Little work was undertaken between 2010 and 2016 until Ardiden acquired the project from Linear Resources in 2016. Further drilling was carried out by Ardiden between 2017 and 2018 resulting in the completion of an updated mineral resource estimate of the Aubry pegmatites in 2018. Ground Penetrating Radar (GPR) was also undertaken by Ardiden in 2018 to test any further exploration potential beyond the current Aubry pegmatite delineating numerous targets.
Geology	- *Deposit type, geological setting and style of mineralisation.*	- **Regional Geology:** The general geological setting of the Seymour Lithium Asset consists of the Precambrian Canadian Shield that underlies approximately 60% of Ontario. The Shield can be divided into three major geological and physiographic regions, from the oldest in the northwest to the youngest in the southeast. - **Local Geology:** The Seymour Lithium Asset is located within the eastern part of the Wabigoon Subprovince, near the boundary with the English River Subprovince to the north. These subprovinces are part of the Superior Craton, comprised mainly of Archaean rocks but also containing some Mesoproterozoic rocks such as the Nipigon Diabase. - **Bedrock Geology:** The bedrock is best exposed along the flanks of steep-sided valleys scoured by glaciers during the recent ice ages. The exposed bedrock is commonly metamorphosed basaltic rock, of which some varieties have well-preserved pillows that have been intensely flattened in areas of high tectonic strain. Intercalated between layers of basalt are lesser amounts of schists derived from sedimentary rocks and lesser rocks having felsic volcanic protoliths. These rocks are typical of the Wabigoon Subprovince, host to most of the pegmatites in the region. - **Ore Geology:** Pegmatites are reasonably common in the region intruding the enclosing host rocks after metamorphism, evident from the manner in

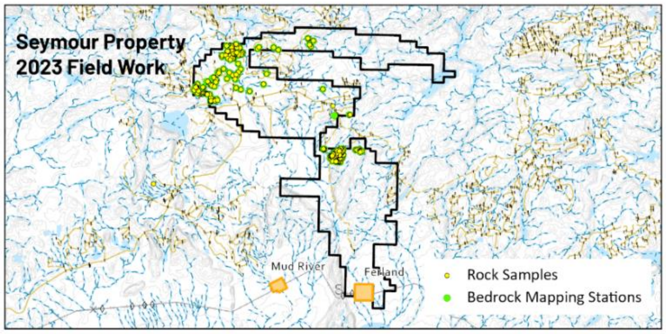
<table>
<tr><th>Criteria</th><th>JORC Code explanation</th><th>Commentary</th></tr>
<tr><td></td><td></td><td>which the pegmatites cut across the well-developed foliation within the metamorphosed host rocks. This post-dating relationship is supported by radiometric dating; an age of 2666 + 6 Ma is given for the timing of intrusion of the pegmatites (Breaks, et al., 2006).
▪ The pegmatites in North Aubry have a northeast plunge direction varying from 10 to 35 degrees from horizontal some 800m downdip extent and 250-300m strike. The North Upper and North Upper high-grade component within, appears to wedge towards the south east and is still open down dip and to the north west.
▪ Southern pegmatites are thinner and less well developed with higher muscovite content and appear to have a more north to north-westerly trend and dip more shallowly to the east. These pegmatites are also hosted in pillow basalts.
▪ The pegmatites are zoned with better developed spodumene crystal appearing as bands, often at an acute angle to the general trend of the pegmatite.
▪ The dominant economic minerals are spodumene with varying proportions of muscovite, microcline, and minor petalite and lepidolite.
▪ The adjacent pillow basalts contain minor disseminated pyrite and pyrrhotite.</td></tr>
<tr><td><i>Drill hole Information</i></td><td><i>▪ A summary of all information material to the understanding of the exploration results including a tabulation of the following information for all Material drill holes:
○ easting and northing of the drill hole collar
○ elevation or RL (Reduced Level – elevation above sea level in metres) of the drill hole collar
○ dip and azimuth of the hole
○ down hole length and interception depth
○ hole length.
▪ If the exclusion of this information is justified on the basis that the information is not Material and this exclusion does not detract from the understanding of the report, the Competent Person should clearly explain why this is the case.</i></td><td>DMS Metallurgy
65 holes within the North Aubry USD2500 pit design were used for metallurgical work, with the following collar coordinates:
<table>
<tr><th>HoleId</th><th>Northing</th><th>Easting</th><th>RL</th><th>Depth</th><th>Azi</th><th>Dip</th></tr>
<tr><td>ASD001</td><td>5585210</td><td>397034</td><td>395</td><td>158</td><td>89</td><td>-89</td></tr>
<tr><td>ASD003</td><td>5585336</td><td>397067</td><td>375</td><td>201</td><td>202</td><td>-73</td></tr>
<tr><td>ASD004</td><td>5585364</td><td>397114</td><td>379</td><td>228</td><td>195</td><td>-71</td></tr>
<tr><td>ASD006</td><td>5585298</td><td>397174</td><td>388</td><td>200</td><td>201</td><td>-75</td></tr>
<tr><td>ASD007</td><td>5585297</td><td>397173</td><td>388</td><td>251</td><td>201</td><td>-85</td></tr>
<tr><td>ASD009</td><td>5585353</td><td>397225</td><td>390</td><td>258</td><td>219</td><td>-85</td></tr>
<tr><td>ASD011</td><td>5585405</td><td>397164</td><td>391</td><td>330</td><td>196</td><td>-86</td></tr>
<tr><td>ASD012</td><td>5585334</td><td>397069</td><td>375</td><td>201</td><td>197</td><td>-54</td></tr>
<tr><td>ASD013</td><td>5585334</td><td>397069</td><td>375</td><td>189</td><td>185</td><td>-61</td></tr>
<tr><td>ASD015</td><td>5585111</td><td>397116</td><td>386</td><td>96</td><td>52</td><td>-85</td></tr>
<tr><td>ASD017</td><td>5585211</td><td>397199</td><td>388</td><td>159</td><td>203</td><td>-69</td></tr>
<tr><td>ASD019</td><td>5585287</td><td>397261</td><td>389</td><td>201</td><td>201</td><td>-70</td></tr>
<tr><td>GTDD-21-0005</td><td>5585400</td><td>397275</td><td>389</td><td>372</td><td>221</td><td>-80</td></tr>
<tr><td>GTDD-22-0001</td><td>5585304</td><td>397013</td><td>379</td><td>201</td><td>273</td><td>-78</td></tr>
<tr><td>GTDD-22-0002</td><td>5585390</td><td>397048</td><td>372</td><td>312</td><td>191</td><td>-75</td></tr>
<tr><td>GTDD-22-0003</td><td>5585451</td><td>397136</td><td>391</td><td>403</td><td>194</td><td>-77</td></tr>
<tr><td>GTDD-22-0010</td><td>5585372</td><td>397400</td><td>389</td><td>395</td><td>224</td><td>-69</td></tr>
<tr><td>GTDD-22-0012</td><td>5585475</td><td>397203</td><td>392</td><td>401</td><td>217</td><td>-81</td></tr>
<tr><td>GTDD-22-0015</td><td>5585475</td><td>397203</td><td>392</td><td>395</td><td>217</td><td>-75</td></tr>
<tr><td>GTDD-22-0093</td><td>5584811</td><td>396621</td><td>345</td><td>220</td><td>220</td><td>-60</td></tr>
<tr><td>GTDD-23-0280</td><td>5585381</td><td>397087</td><td>380</td><td>233</td><td>219</td><td>-60</td></tr>
<tr><td>GTDD-23-0288</td><td>5585535</td><td>397215</td><td>385</td><td>314</td><td>234</td><td>-60</td></tr>
<tr><td>GTDD-23-0443</td><td>5585357</td><td>397195</td><td>391</td><td>242</td><td>219</td><td>-70</td></tr>
<tr><td>GTDD-23-0446</td><td>5585415</td><td>397245</td><td>390</td><td>377</td><td>219</td><td>-69</td></tr>
<tr><td>GTDD-23-0513</td><td>5585114</td><td>397055</td><td>387</td><td>74</td><td>219</td><td>-61</td></tr>
<tr><td>GTDD-23-0565</td><td>5585379</td><td>397288</td><td>387</td><td>251</td><td>214</td><td>-59</td></tr>
</table>
</td></tr>
</table>

Criteria	JORC Code explanation	Commentary

GTDD-23-0632	5585238	397259	388	182	219	-59
GTDD-23-0636	5585317	397327	387	251	219	-59
GTDD-23-0706	5585397	397034	369	266	35	-85
GTDD-23-1028	5584658	396548	335	50	219	-60
GTDD-23-1056	5584616	396594	348	80	220	-59
GTDD-23-1076	5584560	396612	352	77	219	-65
GTDD-23-1122	5584405	396635	374	129	235	-45
GTDD-23-1150	5584394	396667	380	125	219	-60
GTDD-23-1200	5585355	397160	388	242	219	-60
GTDD-23-1203	5585296	396998	382	188	218	-60
SL-16-49	5585113	396997	400	52	271	-60
SL-16-57	5585111	396912	385	50	267	-60
SL-16-58	5585115	396937	387	51	263	-59
SL-16-59	5585095	396915	385	49	275	-61
SL-16-62	5585177	396967	395	105	260	-60
SL-16-63	5585167	396994	397	105	266	-62
SL-16-64	5585238	396998	396	102	263	-59
SL-16-68	5584626	396538	334	52	274	-59
SL-16-72	5585154	396858	378	101	116	-80
SL-17-05	5585107	396913	385	131	94	-61
SL-17-06	5585094	396915	385	111	99	-59
SL-17-11	5585165	396885	378	107	89	-60
SL-17-13	5585208	396887	377	121	88	-61
SL-17-14	5585206	396954	395	118	203	-59
SL-17-21	5585211	397019	396	144	199	-59
SL-17-37	5585267	397008	389	140	211	-60
SL-17-42	5585179	397076	384	123	219	-61
SL-17-50	5585167	397128	389	114	198	-61
SL-17-57	5585230	397133	391	120	191	-62
SL-17-60	5585261	397123	390	129	199	-60
SL-17-62	5585250	397145	393	129	201	-59
SL-17-65	5585265	397186	393	150	203	-60
SL-17-66	5585275	397147	392	141	200	-61
SL-17-67	5585298	397113	389	153	202	-61
SL-17-69	5585317	397100	387	156	199	-61
SL-17-70	5585296	397175	388	156	200	-62
SL-17-71	5585309	397142	386	165	196	-64
SL-17-75	5585125	397130	388	108	264	-63
SL-17-76	5585143	397088	385	81	261	-64

Data aggregation methods	▪ *In reporting Exploration Results, weighting averaging techniques, maximum and/or minimum grade truncations (eg cutting of high grades) and cut-off grades are usually Material and should be stated.* ▪ *Where aggregate intercepts incorporate*	**No drilling is reported in this release.**

Criteria	JORC Code explanation	Commentary
	short lengths of high-grade results and longer lengths of low grade results, the procedure used for such aggregation should be stated and some typical examples of such aggregations should be shown in detail. ▪ *The assumptions used for any reporting of metal equivalent values should be clearly stated.*	
Relationship between mineralisation widths and intercept lengths	▪ *These relationships are particularly important in the reporting of Exploration Results.* ▪ *If the geometry of the mineralisation with respect to the drill hole angle is known, its nature should be reported.* ▪ *If it is not known and only the down hole lengths are reported, there should be a clear statement to this effect (eg 'down hole length, true width not known').*	**No drilling is reported in this release.**
Diagrams	▪ *Appropriate maps and sections (with scales) and tabulations of intercepts should be included for any significant discovery being reported These should include, but not be limited to a plan view of drill hole collar locations and appropriate sectional views.*	**See attached Figures**
Balanced reporting	▪ *Where comprehensive reporting of all Exploration Results is not practicable, representative reporting of both low and high grades and/or widths should be practiced to avoid misleading reporting of Exploration Results.*	**No drilling is reported in this release.**
Other substantive exploration data	▪ *Other exploration data, if meaningful and material, should be reported including (but not limited to): geological observations; geophysical survey results; geochemical survey results; bulk samples – size and method of treatment; metallurgical test results; bulk density, groundwater, geotechnical and rock characteristics; potential deleterious or contaminating substances.*	▪ GT1 completed a fixed wing single sensor magnetic/radiometric/VLF airborne geophysical survey. ▪ Survey details, 1191 line-km, 75m line spacing, direction 90 degrees to cross cut pegmatite strike, 70m altitude. ▪ Final images have been received for Total Count Radiometric, Total Magnetics and VLF from MPX. ▪ Interpretation has been by Southern Geoscience ▪ 100tonne bulk sample of the North Aubry orebody was collected by GT1 in 2023 at 396,950.29E 5,585,061.32N m (UTM NAD83 Z16) ▪ Green Technology Metals conducted geological field investigations and mapping on the Seymour property throughout the second half of the 2023 field season. Efforts were focused on finding new pegmatite occurrences, while mapping the bedrock geology, minerals and structure, across the property. A crew of four collected 194 rock samples and mapped 196 outcrop stations, mainly in the north half of the Seymour property as well as the area immediately NW of the North Aubry deposit. No significant discoveries were made.

Criteria	JORC Code explanation	Commentary
		
Further work	▪ *The nature and scale of planned further work (eg tests for lateral extensions or depth extensions or large-scale step-out drilling).* ▪ *Diagrams clearly highlighting the areas of possible extensions, including the main geological interpretations and future drilling areas, provided this information is not commercially sensitive.*	▪ Further Geological field mapping of anomalies and associated pegmatites at Seymour and regional claims incorporating auger sampling to better test bedrock potential. ▪ Drilling has commenced around neighbouring tenements (Junior Lake) following successful exploration reconnaissance work in 2024. ▪ Continuation of detailed mining studies